

# **Time distribution of adsorption active sites on heterogeneous solid surfaces through experimental measurements of adsorption energies, local adsorption isotherms and the energy distribution function by reversed-flow gas chromatography**

## **Research Team**

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## **Introduction**

The Reversed Flow – Gas Chromatography (RF-GC) is a well known dynamic method combining simplicity with accuracy Katsanos [5] and Katsanos et al. [6]. This method is useful especially for complex systems, where surface heterogeneity plays a very important role and must be taken into account in the physicochemical interpretation of the adsorption process, Metaxa et al.[13], Kalogirou et al.[3]. This method based on two mass-balance equations, one in the gas region and the other in the solid bed one, is useful for evaluating adsorption isotherms because it gives model-independent results, Sotiropoulou et al. [20]. The RF-GC method is also described and evaluated for the determination of many physicochemical parameters in homogeneous gas phase, Roubani-Kalantzopoulou et al.[14] and in heterogeneous as well, Yun et al. [22], Karagiorgos et al. [4] and Birbatakou et al. [1].

The RF-GC method has been applied recently for the measurement of some local parameters concerning adsorption energies,  $\varepsilon$ , with respect to time, Katsanos et al.[7,8], gaseous adsorbate concentrations above the solid surfaces,  $c_y$ , local monolayer capacities,  $c_{\max}^*$ , that is the maximum adsorbed concentrations of the probe gases on the collection of the adsorption sites  $i$  being active at time  $t$  and local adsorption isotherms,  $\theta_i(p, T, \varepsilon)$ , Roubani-Kalantzopoulou et al. [15]. In addition, the probability density function,  $\varphi(\varepsilon)$ , Roubani-Kalantzopoulou et al. [16] (a modified function, of the former  $f(\varepsilon)$ , Katsanos et al.[9] and Siokos et al. [19], of adsorption energies for some probe gases on heterogeneous solid surfaces, as well as the lateral molecular interaction energies (dimensionless),  $\beta\theta_i$ , have been determined through the same experimental results, Katsanos et al.[10]. The term “local” means with respect to time, that is involves only a limited collection of adsorption sites active at time  $t$ .

This article concerns adsorption occurring at gas-solid interfaces, when the solids are heterogeneous in nature, as well determination of adsorption energies and related parameters of seven gaseous substances (five organic in the presence or not of an

inorganic, O<sub>3</sub> or NO<sub>2</sub>) on ten heterogeneous solid adsorbents. Thus, a time resolved chromatographic study is done for the characterization of all these gas-solid interfaces.

## Experimental

The experimental set-up and the procedure can be found in the invited review article written recently by Roubani- Kalantzopoulou [17].

The light hydrocarbons, C<sub>2</sub>H<sub>2</sub>, C<sub>2</sub>H<sub>4</sub>, C<sub>2</sub>H<sub>6</sub>, C<sub>3</sub>H<sub>6</sub> and 1-C<sub>4</sub>H<sub>8</sub>, as well as the nitrogen dioxide, were obtained from Air Liquide and had a purity of 99.000%-99.999%. The carrier gas was nitrogen 99.999% from Air Liquide, dried by silica gel. Ultra-high-purity hydrogen from the same company was also used as reactant as well as carrier gas for the study of heterogeneous catalytic reactions.

The O<sub>3</sub> was prepared in the laboratory by using a laboratory ozonizer (Ozoneur OZ1-L of OZONIA Int.) and had a concentration of 3.3 g/Nm<sup>3</sup>.

The solids Cr<sub>2</sub>O<sub>3</sub>, CdS, TiO<sub>2</sub> and PbO<sub>2</sub> were pro-analysis products of Merck. The solids ZnS, CaO, MgO and SiO<sub>2</sub> were products of Fluka with a high purity (>99%).

The catalysts used in catalytic studies were NiO black from Fluka (nickel content: ~76%), and Co<sub>3</sub>O<sub>4</sub> from Merck (cobalt content: ~80%).

## Theory

The RF-GC method does not depend on analytical or numerical solutions of the classical integral Eq. (1) (cf. Refs Margariti et al. [11,12]), Tyllipaki et al.[21], Roubani-Kalantzopoulou et al. [17], but on a time function of the extra chromatographic peaks obtained by short flow-reversals of the carrier gas, as Eq. (2) shows:

$$\Theta(p, T) = \int_0^{\infty} \theta_i(p, T, \varepsilon) f(\varepsilon) d\varepsilon \quad (1)$$

$$H^{1/M} = gc(l', t) = \sum_{i=1}^4 A_i \exp(B_i t) \quad (2)$$

where  $\Theta(p, T)$  is the overall experimental adsorption isotherm,  $\theta_i(p, T, \varepsilon)$  the local isotherm,  $f(\varepsilon)$  the probability density function for the adsorption energies,  $H$  is the peak height,  $M$  the response factor of the detector,  $A_i$  the pre-exponential factors, and  $B_i$  the exponential coefficients of time  $t$ , when flow reversals were performed.

The main equation of the experimental technique as well as of the corresponding model is Eq. (2). The relevant mathematical model with the calculation of  $A_i$  and  $B_i$  values from the experimental points  $H$ ,  $t$ , and their physical content have been reported many times.

Finally, the necessary relations for the calculation of  $\varepsilon$ ,  $c_{\max}^*$ ,  $\theta_1(\theta_t)$ ,  $\varphi(\varepsilon)$  and  $\beta$  from Eq. (2), for the adsorption of gases on heterogeneous surfaces as a function of time, have been obtained through the combination of Eq. (2) and the Jovanovic isotherm model written in the form as Eq. (10) of Ref. [7] shows:

$$\theta(p, T, \varepsilon) = 1 - \exp(-K p) \quad (3)$$

where

$$K = K^0(T) \exp(\varepsilon / RT) \quad (4)$$

$R$  being the gas constant, and

$$K^0 = \frac{h^3}{(2\pi m)^{3/2} (kT)^{5/2}} \cdot \frac{u_s(T)}{b_g(T)} \quad (5)$$

Here,  $K$  is the Boltzmann's constant;  $m$  the molecular mass of the adsorbate,  $h$  the Planck's constant and  $u_s(T)/b_g(T)$  the ratio of two partition functions, namely the one for the adsorbed molecule,  $u_s(T)$ , and that for the rotations-vibrations in the gas phase  $b_g(T)$ . This ratio equals approximately one.

More precisely, the relations for the calculation of  $\varepsilon$  (kJ mol<sup>-1</sup>),  $c_{\max}^*$  (mol g<sup>-1</sup>) and  $\theta_t$  from experimental data are given by Eqs (6)-(8):

$$\varepsilon = RT \left[ \ln(KRT) - \ln(RT) - \ln K^0 \right] \quad (6)$$

$$c_{\max}^* = c_s^* + \frac{1}{KRT} \cdot \frac{\partial c_s^*}{\partial c_y} \quad (7)$$

$$\theta_t = 1 - \frac{1}{c_{\max}^*} \cdot \frac{1}{KRT} \cdot \frac{\partial c_s^*}{\partial c_y} \quad (8)$$

According to Jaroniec and Madey [17], the probability density function  $f(\varepsilon)$  of Eq. (1) describing the adsorption energy distribution, is defined as the derivative of the number of adsorption sites with respect to the adsorption energy. Since the number of adsorption sites is proportional to the local monolayer capacity  $c_{\max}^*$  of Eq. (7),  $f(\varepsilon)$  may be defined as:

$$f(\varepsilon) = \frac{\partial c_{\max}^*}{\partial \varepsilon} = \frac{\partial c_{\max}^* / \partial t}{\partial \varepsilon / \partial t} \quad (9)$$

Finally one obtains [23]:

$$f(\varepsilon) = \frac{1}{RT} \left[ \frac{KRT(\partial c_s^* / \partial t) + \partial^2 c_s^* / \partial c_y \partial t}{\partial(KRT) / \partial t} - \frac{\partial c_s^* / \partial c_y}{KRT} \right] \quad (10)$$

The modified function  $\varphi(\varepsilon)$  is produced if  $f(\varepsilon)$  is multiplied by  $\theta$  and the product divided by  $c_{\max}^*$ .

$$\varphi(\varepsilon; t) = \theta f(\varepsilon) / c_{\max}^* \quad (11)$$

As regards the lateral interactions of the adsorbed molecules, the dimensionless parameter  $\beta$  Margariti et al.[12] can be obtained:

$$\beta = z\omega / RT \quad (12)$$

$\omega$  being the lateral interaction energy and  $z$  the number of neighboring atoms for each adsorption site. Thus, the  $\theta z\omega$  is the differential energy of adsorption added to  $\varepsilon$  due to lateral interactions.

## Results and discussion

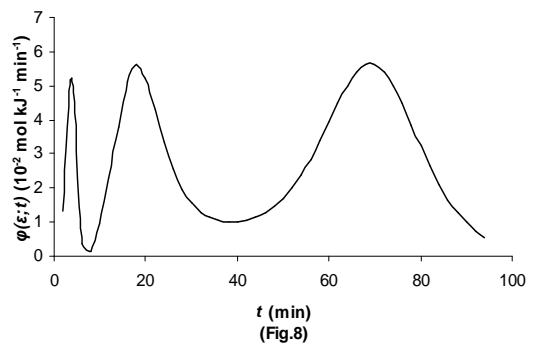
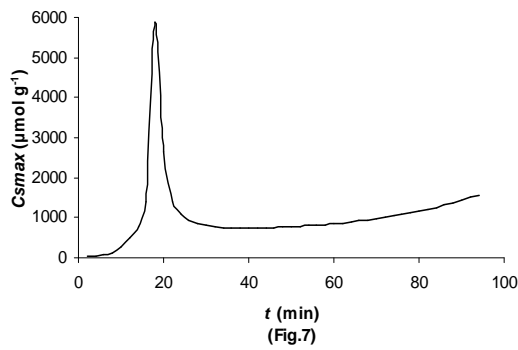
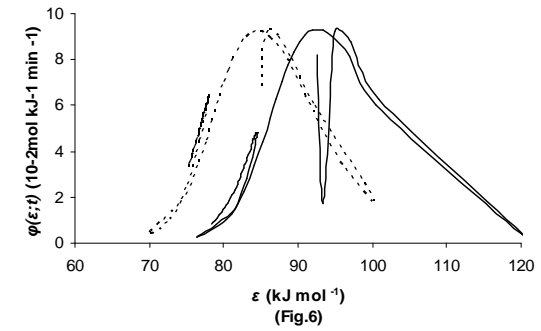
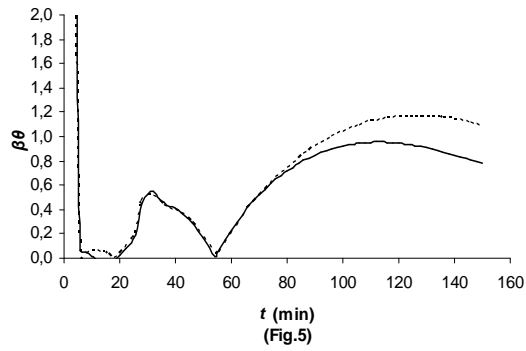
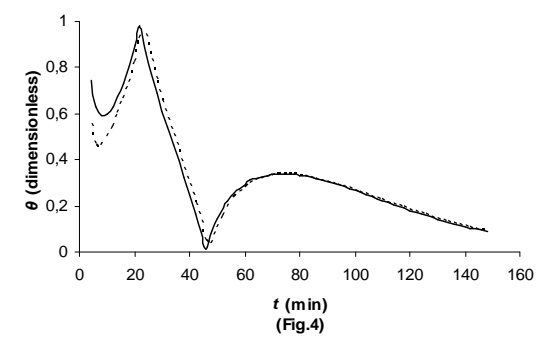
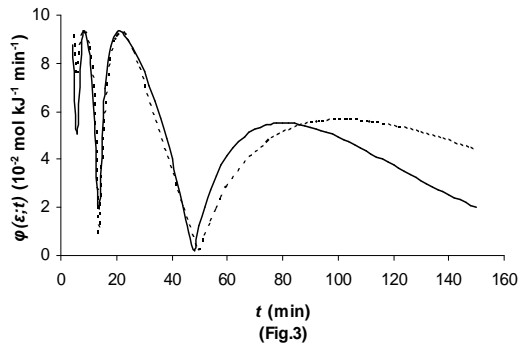
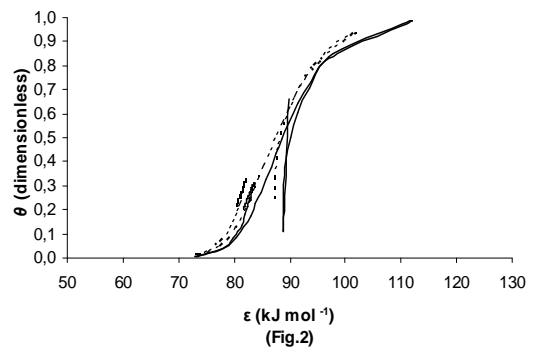
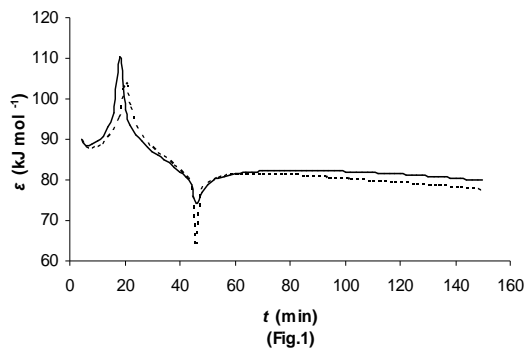
The calculations of the new physicochemical quantities  $\varepsilon$ ,  $c_{\max}^*$ ,  $\theta_i$ ,  $\varphi(\varepsilon)$  and  $\beta$  pertaining to heterogeneous surfaces, start from the diffusion bands of RF-GC experiments {cf. Refs [1, 17]} by recording the pairs  $H$ ,  $t$  and calculating the pre-exponential factors  $A_1$ ,  $A_2$ ,  $A_3$  and  $A_4$ , and the time coefficients  $B_1$ ,  $B_2$ ,  $B_3$  and  $B_4$ . By entering the pair values of  $H$ ,  $t$  into the DATA lines of a non-linear regression analysis GW- PC program the physicochemical parameters and functions exposed and defined in the section Theory are calculated and printed. The adsorption energy  $\varepsilon$  versus experimental time, for the systems propylene/chromium oxide and propylene/ozone/chromium oxide (dot line) at 323.2 K, in nitrogen atmosphere is presented in Fig. 1. The gas molecules at time  $t$  are exclusively adsorbed on sites  $i$  all of the same energy  $\varepsilon_i$ . The maxima and minima represent rather transition adsorption energies before their final leveling off with time.

The local adsorption isotherm,  $\theta_i$ , versus adsorption energy,  $\varepsilon_i$ , for the systems propylene/zinc sulfide and propylene/ozone/zinc sulfide (dot line) at 323.2 K, in nitrogen atmosphere is shown in Fig. 2. The shape of these curves resembles that given by Adamson and Ling, as exemplified by Rudzinski and Everret [18]. The main difference is that, in this case, all the physicochemical quantities are obtained experimentally and not analytically.

Concerning the dependence of distribution function of adsorption energies on the experimental time for the systems ethane/cadmium sulfide and ethane/ozone/cadmium sulfide (dot line) at the same conditions as above, three types of adsorption active sites are evident, Fig. 3. It's impressive that similar results can be carried out from the corresponding plot in Fig. 8, concerning the heterogeneous catalytic hydrogenation of 1-butene on nickel oxide catalytic bed at 260 °C.

The lateral molecular interaction energy  $\beta\theta_i$  (dimensionless) as a function of time for the system 1-butene/(ozone)/silicon oxide in Fig. 5 shows that a similar behavior is observed and the plots also show three kinds of active sites for adsorption. The same results are obtained from the plots in Fig. 4, where a time resolved analysis regarding local isotherms is presented for the system 1-butene/(ozone)/chromium oxide.

The dependence of distribution function of adsorption energies in relation with the adsorption energies themselves for the systems ethylene/magnesium oxide and ethylene/ozone/magnesium oxide at 323.2 K is presented in Fig. 6. A Gaussian curve is observed (the slight deviations from this behavior correspond to the beginning and the end of the experimental results). In Fig. 7, the time resolved analysis of the local monolayer capacities,  $c_{\max}^*$ , is strongly depending on the experimental temperature.



**Figures 1-8** . Physicochemical quantities for surface characterization of gas-solid interfaces, through a suitable time -resolved chromatographic analysis.

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